

Heat and Mass Transfer (DI05019071)

Complete Lecture Deck

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Equimolar Counter Diffusion & Convective Mass Transfer

- Course: Heat and Mass Transfer (DI05019071)
- Unit 5: Mass Transfer
- Lecture 45: Equimolar Counter Diffusion & Convective Mass Transfer

Lecture Agenda

- 1. What is Equimolar Counter Diffusion?
- 2. Derivation of Flux for Equimolar Counter Diffusion
- 3. Concentration Profile
- 4. Introduction to Convective Mass Transfer (Topic 5.6)
- 5. The Mass Transfer Coefficient
- 6. Dimensionless Numbers (Sh, Sc, Le)
- 7. Course Wrap-up

Equimolar Counter Diffusion: Concept

- Occurs in binary gas mixtures (A and B) where the molar fluxes of A and B are equal in magnitude but opposite in direction.
- Condition: $N_A = -N_B$
- Therefore, total molar flux $N = N_A + N_B = 0$.
- Physical example: Distillation processes, or two large tanks containing different ideal gases connected by a tube at constant pressure and temperature.

Governing Equation (Equimolar)

- Recall the total absolute molar flux equation:
- $N_A = -D_{AB} * (dC_A / dx) + x_A * (N_A + N_B)$
- Since $N_A = -N_B$, the bulk convective term $(N_A + N_B)$ is zero.
- Thus, $N_A = -D_{AB} * (dC_A / dx)$
- Conclusion: In equimolar counter diffusion, the total absolute flux is exactly equal to the diffusion flux. The bulk mixture is strictly stationary (molar-average velocity $V = 0$).

Flux and Concentration Profile (Equimolar)

- Since N_A is constant (steady state), integrating Fick's law over length L gives:
- $N_A = D_{AB} * (C_{A1} - C_{A2}) / L$
- For ideal gases, $C_A = p_A / (R_u * T)$. Substituting this:
- $N_A = D_{AB} * (p_{A1} - p_{A2}) / (R_u * T * L)$
- The concentration (and partial pressure) profile is linear across the diffusion path.

Convective Mass Transfer (Topic 5.6)

- When mass transfer occurs between a surface and a moving fluid, it involves both diffusion and bulk fluid motion.
- Analogous to convective heat transfer (Newton's Law of Cooling).
- The flow regime (laminar or turbulent) heavily influences the mass transfer rate.
- A concentration boundary layer develops over the surface.

The Mass Transfer Coefficient (h_m)

- Convective mass transfer rate is governed by an equation analogous to Newton's Law of Cooling.
- Rate equation: $N_A = h_m * (C_{A,surface} - C_{A,infinity})$
- Where:
 - - N_A = Molar convective flux ($\text{kmol}/\text{m}^2 \cdot \text{s}$)
 - - h_m = Convective mass transfer coefficient (m/s)
 - - $C_{A,surface}$ = Concentration at the surface
 - - $C_{A,infinity}$ = Free stream concentration

Finding h_m : Dimensionless Numbers

- Like 'h' in heat transfer, ' h_m ' is difficult to calculate analytically. We rely on empirical correlations using dimensionless numbers.
- In heat transfer, we used Nusselt $(Nu) = f(\text{Reynolds}, \text{Prandtl})$.
- In mass transfer, we use Sherwood $(Sh) = f(\text{Reynolds}, \text{Schmidt})$.

Sherwood and Schmidt Numbers

- **Sherwood Number (Sh)**: Ratio of convective mass transfer to mass diffusion.
- $Sh = (h_m * L_c) / D_{AB}$ [Analogue to Nusselt Number]
- **Schmidt Number (Sc)**: Ratio of momentum diffusivity to mass diffusivity.
- $Sc = \nu / D_{AB} = \mu / (\rho * D_{AB})$ [Analogue to Prandtl Number]
- Typical Correlation: $Sh = C * Re^m * Sc^n$

The Lewis Number (Le)

- ****Lewis Number (Le)****: Links heat and mass transfer. It is the ratio of thermal diffusivity to mass diffusivity.
- $Le = \alpha / D_{AB} = Sc / Pr$
- Significance:
 - - If $Le = 1$, thermal and concentration boundary layers grow at the exact same rate.
 - - For many gas mixtures (like water vapor in air), Le is approximately 1, simplifying simultaneous heat and mass transfer analysis.

Summary of Mass Transfer

- Equimolar counter diffusion occurs when two species diffuse in opposite directions at equal molar rates ($N_A = -N_B$).
- Convective mass transfer is analogous to convective heat transfer.
- The mass transfer coefficient (h_m) is determined using the Sherwood and Schmidt dimensionless numbers.
- The heat and mass transfer analogy is a powerful engineering tool.

Course Conclusion

- This concludes the Heat and Mass Transfer course (DI05019071).
- We have covered:
 - - Conduction (Fourier's Law)
 - - Convection (Newton's Law of Cooling)
 - - Radiation (Stefan-Boltzmann Law)
 - - Heat Exchangers
 - - Mass Transfer (Fick's Law)
- Best of luck with your final examinations!